

# Membrane Modeling In Carbon Capture Technology

Kriti Gupta<sup>1</sup>, Paul-Christiaan Spruijtenburg<sup>1</sup>, Bryan Verveld<sup>1</sup>

<sup>1</sup>Demcon Multiphysics B.V.

## Abstract

Aqualung Carbon Capture [1] provides membrane modules that capture carbon, to aid in the decarbonization of heavy industry and transport. These modules filter CO<sub>2</sub> from process gas streams with minimal additional pressure drops. We supported Aqualung by aiding in the improvement of a membrane module containing more than 2000 filtering fibers. Using the CFD module in COMSOL we calculated the efficiency of the module for different geometries.

In Figure 1, the flow process and the modelling concept are shown. CO<sub>2</sub> rich inflow enters the membrane module, passes through the membrane fibers where CO<sub>2</sub> is absorbed, thus the outflow is deplete in CO<sub>2</sub>. In order to simulate CO<sub>2</sub> filtering, two physical processes are of importance: (1) the pressure drop within the module and through the fibers, (2) the microscopic process of membrane filtering that depends on the concentration ratio of CO<sub>2</sub> within the module vs within the fibers. Because the geometries can contain up to 2000 fibers, the simulation in COMSOL is simplified by splitting the system into two effective porous media: module and fibers.

For each medium, the interface 'Free and porous media flow, Brinkman' is used to calculate the velocity and pressure fields. The local concentrations in each medium are calculated using the interface 'Transport of concentrated species'. The coupling between the two interfaces is done using the Multiphysics 'Reacting flow' feature. The concentration and fluid flow are coupled using the Multiphysics coupling 'Reacting flow'. Finally, the CO<sub>2</sub> exchange between the two media: module and the fiber are coupled using a concentration and pressure dependent sink and source term respectively.

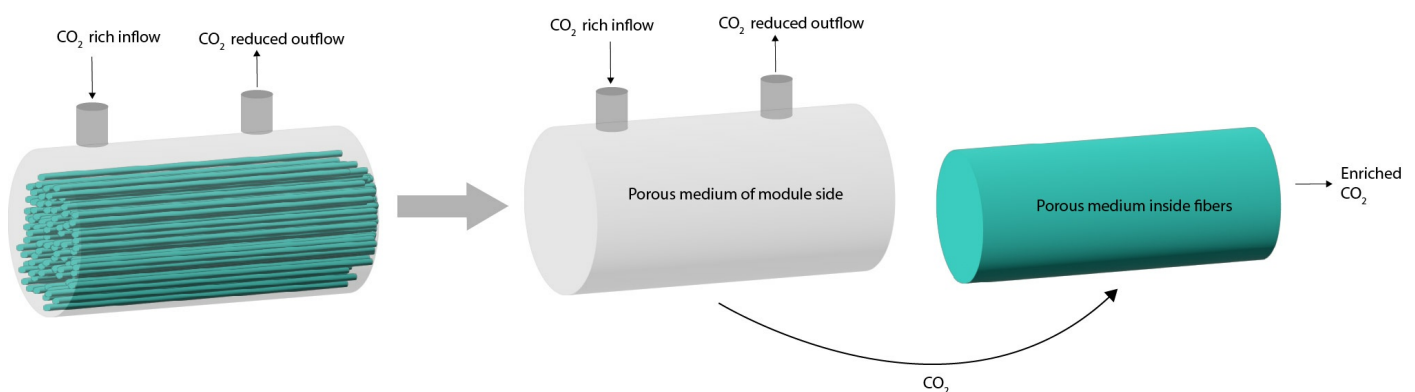
The result of the simulation, when applying all above mentioned boundary conditions, can be seen in Figure 2. The concentration of CO<sub>2</sub> on the module side decreases across the module. At the same time, the CO<sub>2</sub> emerges on the fiber side, locally increasing the concentration before flowing out of the module. This indicates that the module is working as intended and is extracting CO<sub>2</sub> from the feed flow.

Using CFD simulations, input parameters such as module geometry, fiber packing density, and process parameters can be quickly iterated to optimize the module. This means that the module can be tuned for specific industrial processes. In this way, a cost-benefit analysis can be performed, assessing CO<sub>2</sub> capture purity and CO<sub>2</sub> mass flow on the one hand, and the costs such as pumping power and size of the module on the other hand.

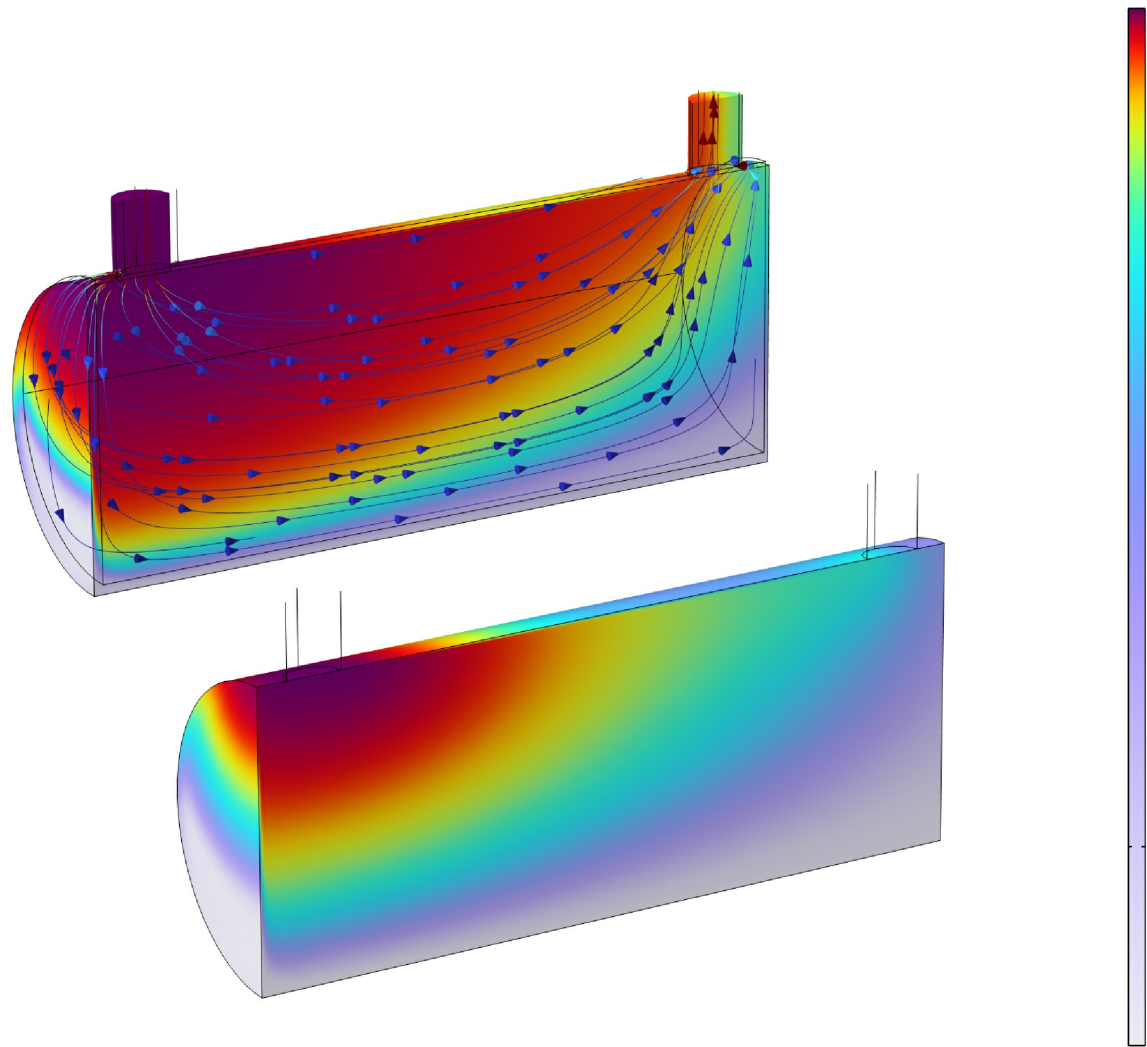
## Reference

[1] <https://aqualung-cc.com/>

## Figures used in the abstract



**Figure 1** : Left: actual geometry with the fibers inside the module. Right: simulation concept. The module and the fibers are modelled as two porous media and coupled with a CO<sub>2</sub> term.



**Figure 2** : Top: the module domain, bottom: the fiber domain. The arrows in the module domain represent the flow profile on the module side. The color represents the mass fraction of CO<sub>2</sub>.