Optimization of the Gas Flow in a GEM Tracker with COMSOL and TENDIGEM Development



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Presented at the 2011 COMSOL

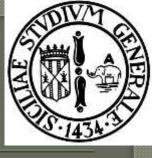
Conference



V. Bellini, E. Cisbani, V. De Smet, F. Librizzi, F. Mammoliti, F. Noto, C. Sutera



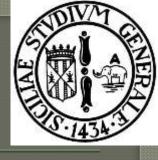
Overview



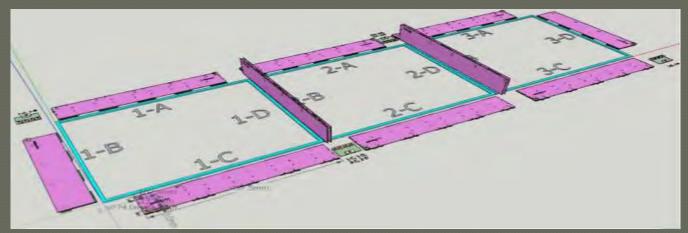
- 1. Introduction
 - The triple-GEM detector
- 2. Study and optimization of the gas system
- 3. Tendigem developement
- 4. Conclusion



1 Introduction



- The GEM (Gas Electron Multiplier) chambers is currently under development
 - •Front Tracker:
 - two 10 x 20 cm² silicon strip planes
 - six 40 x 150 cm² GEM chambers (each made up of three adjacent 40 x 50 cm² triple-GEM modules)
- •Energy upgrade of the Jlab CEBAF (Continuous Electron Beam Accelerator Facility): up to 11 GeV in Hall A (2014)





The triple-GEM detector



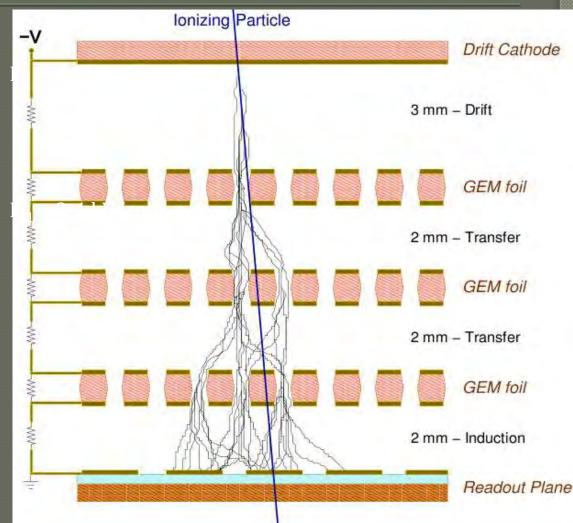
• Working Principle

Ionization by the charged particle

Charge multiplication in holes of GEM foils

Drift of electrons in induction gap induce signal on the anode read-out

Excellent intrinsic spatial resolution: ~40 µm RMS



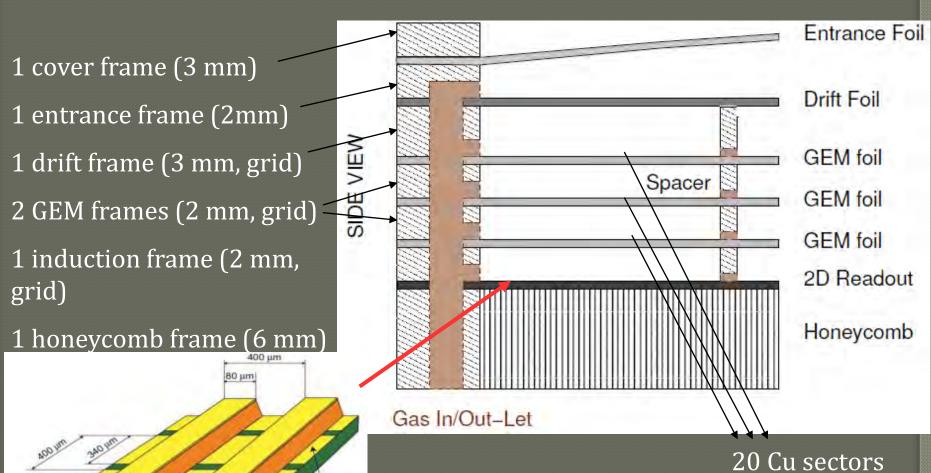


Insulating layer

Readout strips (top layer)

The triple-GEM detector





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Readout strips

Support

 $20 \times 5 \text{ cm}^2$



The triple-GEM detector



GEM foil

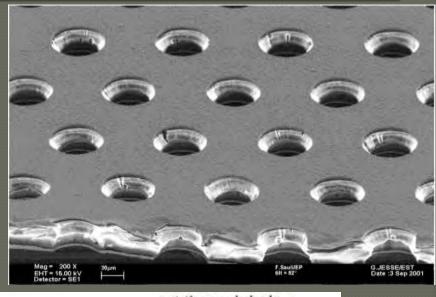
50µm insulating Kapton coated on both sides with 3 to 5 µm Cu

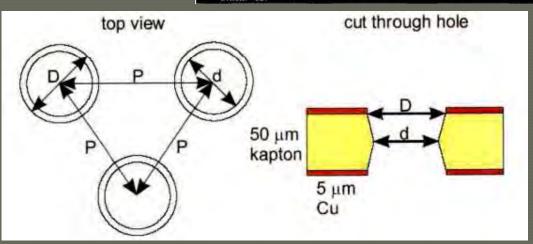
Densily perforated:

 $D = 70 \mu m$

 $d = 50 \mu m$

 $P = 140 \mu m \text{ (Lead)}$







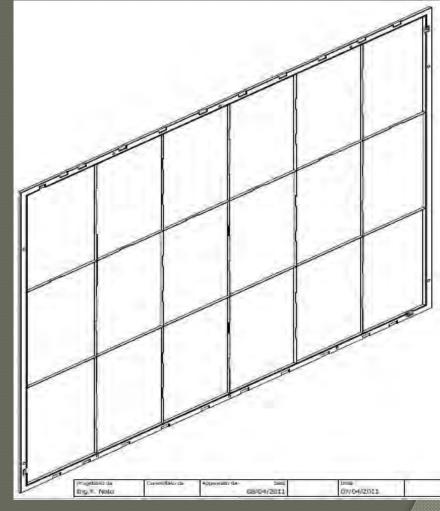
Study and optimization

of the gas system



- Optimization of the GEM frame design
- 2 main goals:
- Improve gas flow uniformity: by optimizing the design of the grid in the frame
 - ⇒ Study performed with:

 - a géometry defined in 2D Thin-Film Flow Model Model of 1 single frame as if its volume were delimited by 2 solid walls
- Avoid turbulence: by optimizing the diameter of the tubes leading to the inlets and outlets by optimizing the design of the inlets and outlets





Method



 Finite Element Method using COMSOL Multiphysics

• 2D Geometry & Thin-Film Flow Model

film thickness: 2 mm in sectors

1 mm in grid openings, inlets and outlets

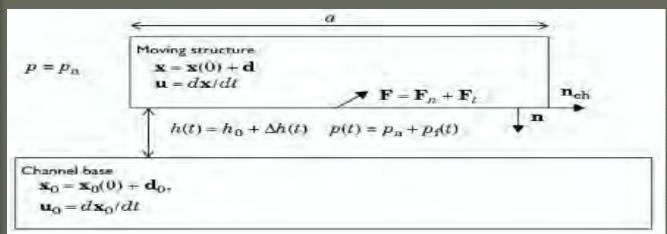
 Choice of model & mesh design: influenced by requiring computational capacity



Method(2)



Thin-Film Flow Model:



CFD Module User's Guide v4.1, COMSOL AB, 2010.

- The film thickness *h* remains very small respect to the dimensions of solid structures
- The channel curvature is small
- The inertial effects in the fluid are negligible compared to the viscous effects, thus the flow is laminar.
- The pressure p = pa + pf is constant over the film thickness h.
- The velocity profile over the film thickness is parabolic.
- The fluid is isothermal





• Reynolds equation:

$$\frac{\partial(\rho b)}{\partial t} + \overrightarrow{\nabla}_{tg} \cdot (\rho h \vec{U}) - \rho (\overrightarrow{\nabla}_{tg} \Delta h_m \cdot \vec{u}_m - \overrightarrow{\nabla}_{tg} \Delta h_b \cdot \vec{u}_b) = 0$$

$$\vec{U} = -\frac{\overrightarrow{\nabla}_{tg}p}{12\mu}h^2Q_{ch} + \frac{\overrightarrow{u_m} + \overrightarrow{u_b}}{2}$$

- 3 volume renewals per hour => total inlet flow 60 cm³/min
- constant density $r=1.8417 \text{ kg/m}^3$ $(U_s=314 \text{ m/s} >> U_i=0.0625 \text{ m/s})$
- constant dynamic viscosity m=1.9696 · 10-5 Pa.s (Reichenberg's formula)
- immobile solid structures: h constant, $Dh_m = Dh_b = u_m = u_b = 0$
- continuum => Q_{ch} = 1





• Reynolds equation:

$$\overrightarrow{\nabla}_{\mathrm{tg}} \cdot \overrightarrow{\nabla}_{\mathrm{tg}} p_f = 0$$

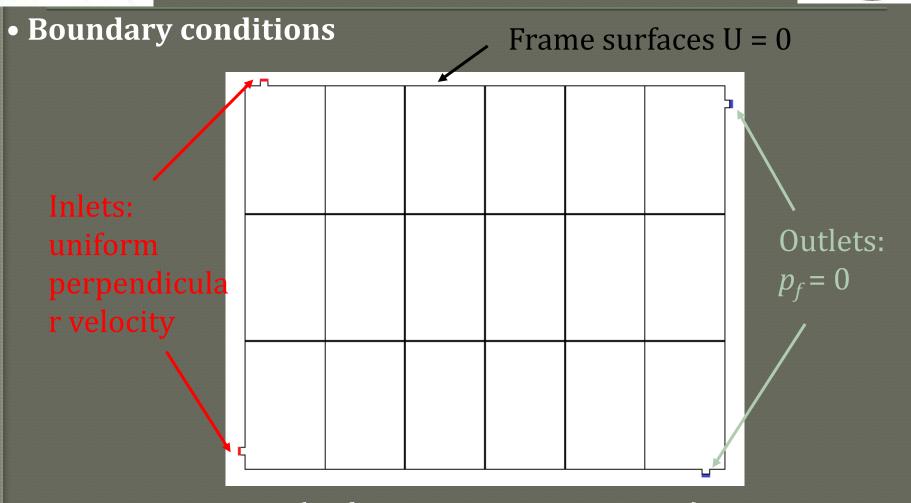
$$\vec{U} = -\frac{h^2}{12\mu} \overrightarrow{\nabla}_{tg} p_f$$

independent of p_a and p_a

- 3 volume renewals per hour => total inlet flow 60 cm³/min
- constant density $r=1.8417 \text{ kg/m}^3$ $(U_s=314 \text{ m/s} >> U_i=0.0625 \text{ m/s})$
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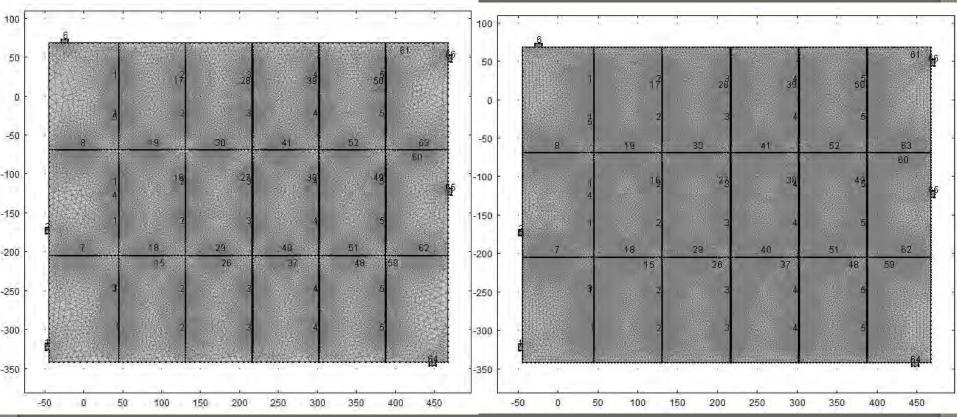


(ambient pressure $p_a = 1$ atm)





Mesh Quality



Mesh with only 1 predefined

« size »: Fine

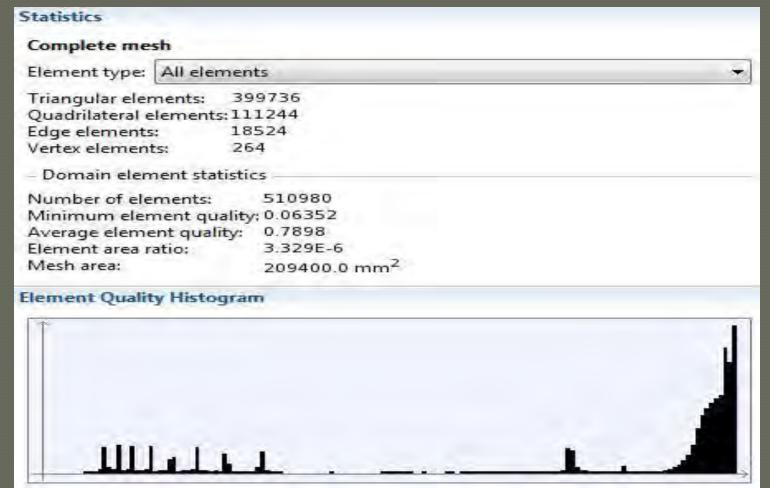
Mesh with only 1 predefined

« size » : Extra fine





Extra fine Mesh Quality







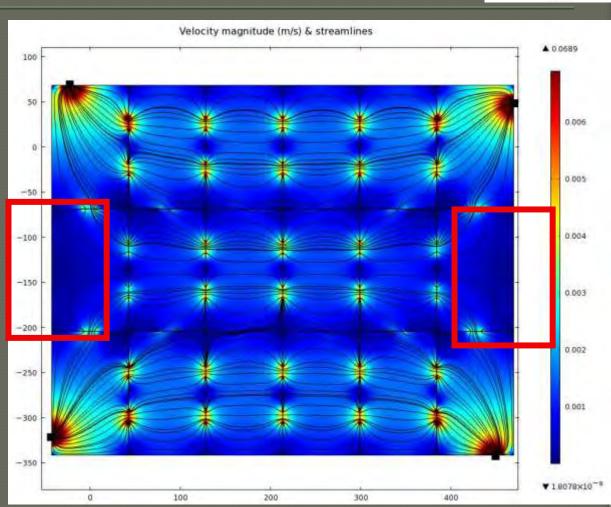
Prototype version:

2 inlets $(U_i = 0.0625 \text{m/s})$

2 outlets

18 sectors

2 large low flux zones







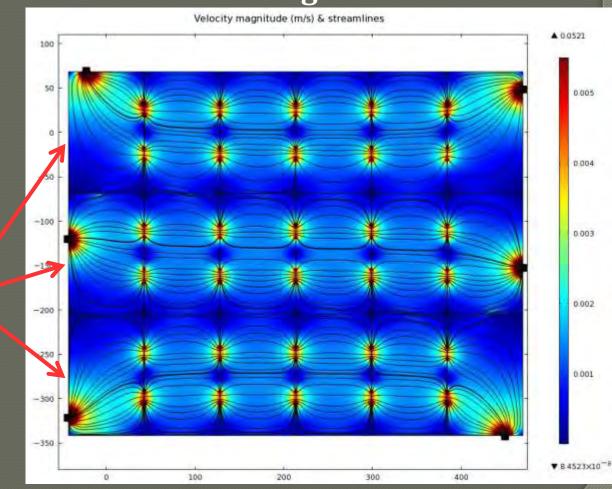
Modified inlet and outlet configuration

3 inlets $(U_i = 0.04167 \text{m/s})$

3 outlets

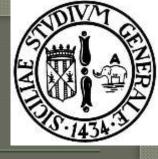
18 sectors

Six-sector rows: 3 independent and similar flows





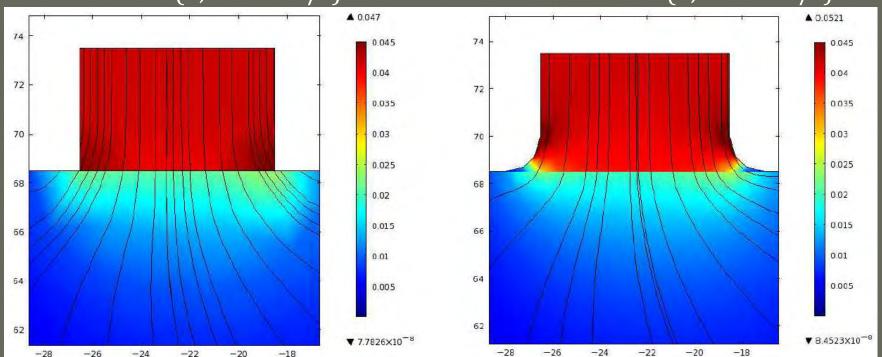
Simulation 2 (continued)



Modified inlet and outlet configuration



Simulation 2 (0,04167 m/s)



circular joints 1.5 mm radius at inlets & outlets

=> slight reduction of the high velocities inside sector

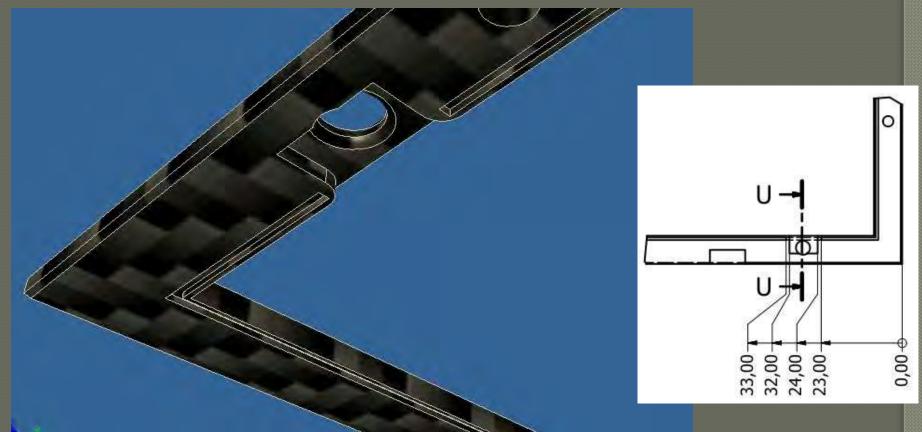
& stabilization of the boundary layers



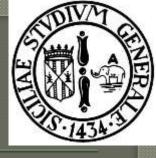
Simulation 2 (continued)



Modified inlet and outlet configuration







Reduction from 18 to 12 sectors:

The idea is to reduce the number of vertical spacers in order to have less «dead angles» (the velocity of the gas is too slow in these corners)

Planarity of the GEM foils

Normal pressure

 10 N/m^2

$$u_{\text{max}} = \kappa(\zeta) \frac{PS}{T}$$

Maximum sector area: 265 cm²

 $20 \mu m$

Maximum deformation

< 0.074

Geometrical factor

9.81 N/cm

Circumference force per unit length

(sector area = 222 cm^2)

⇒ Minimum number of sectors: 9

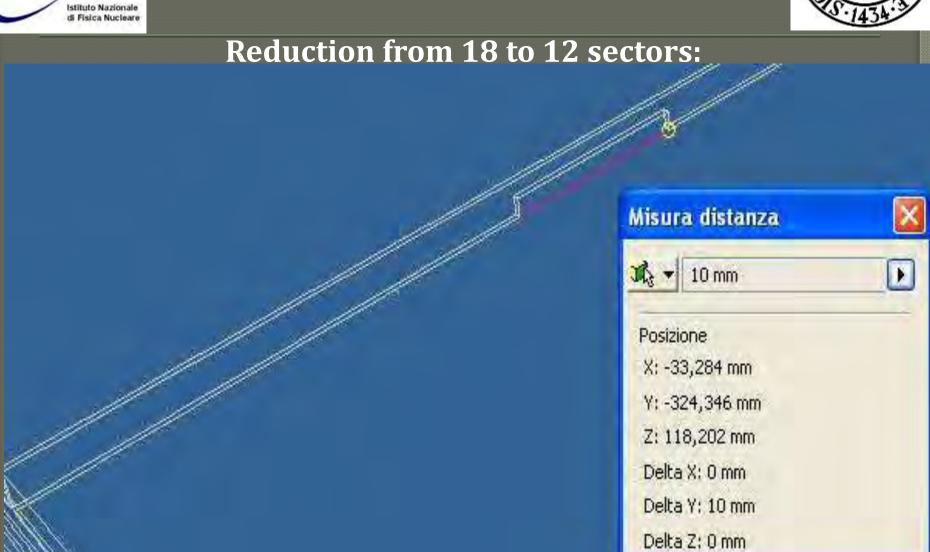
Conservative choice: 12 sectors

(sector area = 166 cm^2)



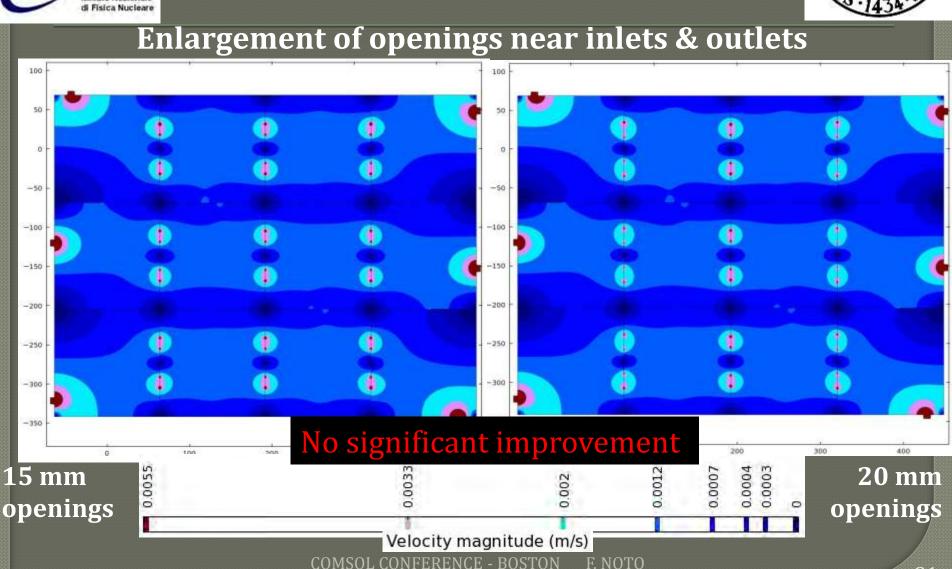
Simulation 3 (continued)





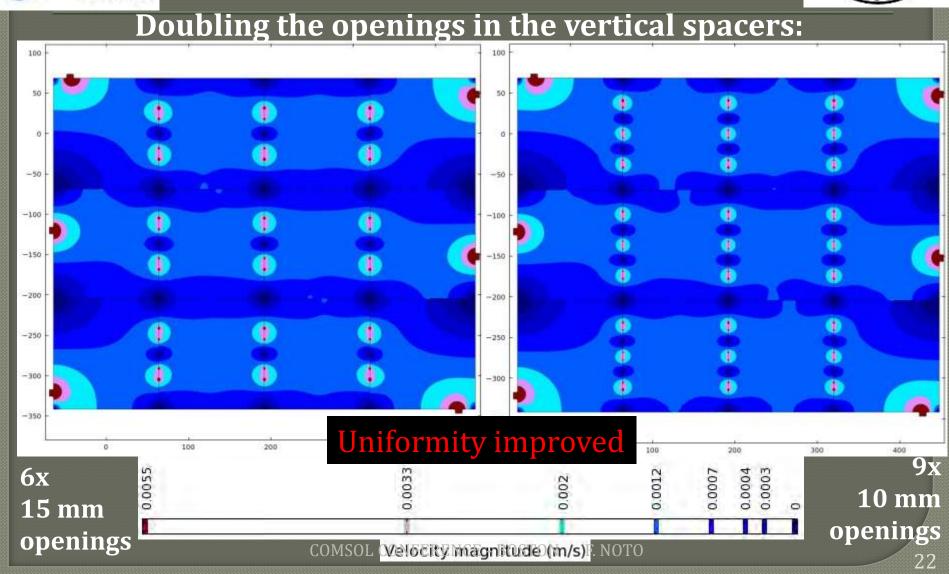








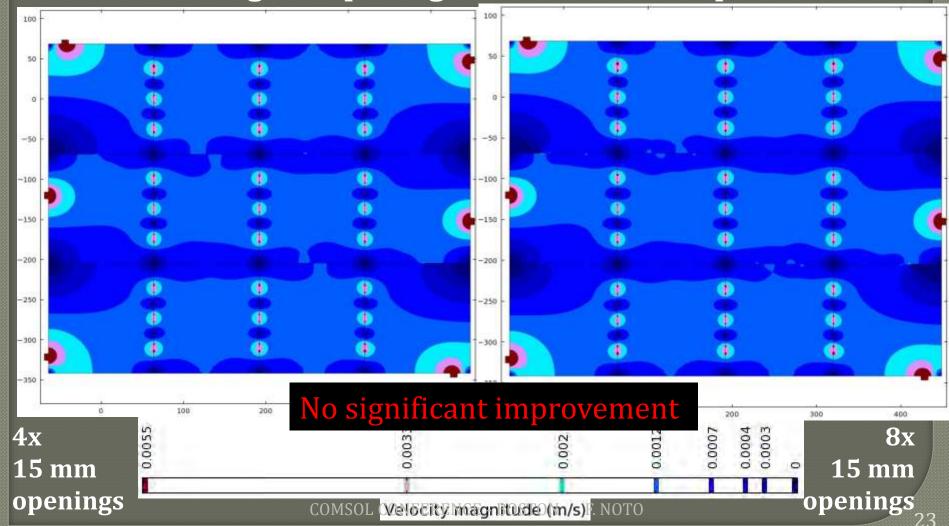










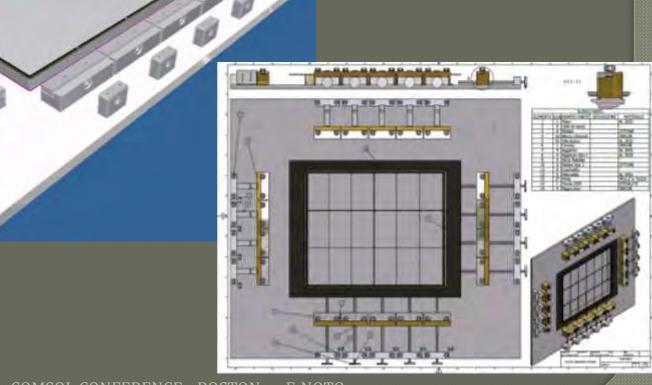




TENDIGEM



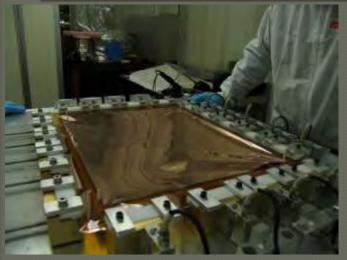






TENDIGEM





Stretching









Conclusion



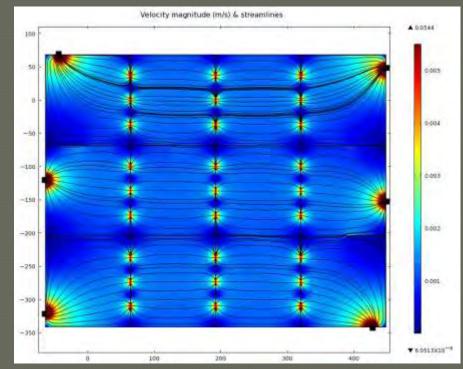
Study and optimization of the gas system

· Significant improvement of the gas flow uniformity in the

2 mm gap between 2 GEM foils of a 40 x 50 cm² module

Final frame design:

- 3 inlets and 3 outlets (with circular joints)
- 12 sectors
- vertical spacers:9 openings of 10 mm
- orizontal spacers:4 openings of 15 mm



 Inlet and outlet pipes cause a very large fraction of the total pressure loss in a 40 x 50 cm² module

Thank you for your attention